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⑯ Zeolite EU-1.

⑯ A new zeolite material designated EU-1 having a
molar composition expressed by the formula:0.5 to 1.5 R₂O : Y₂O₃ : at least 10 XO₂ : 0 to 100 H₂O

wherein R is a monovalent cation or 1/n of a cation of
valency n, X is silicon and/or germanium, Y is one or
more of aluminium, iron, gallium or boron, and H₂O is
water of hydration additional to water notionally present
when R is H, and having an X-ray pattern substantially
as set out in Tables 1 and 2 is prepared from a reaction
mixture containing XO₂ (preferably silica), Y₂O₃ (prefer-
ably alumina) and a dicationic alkylated polymethylene
diamine. The new zeolite is useful in catalytic pro-
cesses, especially xylenes isomerisation.

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ZEOLITE EU-1

The present invention relates to a zeolite material, hereinafter referred to as zeolite EU-1, to a method of making it and to processes using it as a catalyst.

According to the present invention we provide

5 zeolite EU-1 having a molar composition expressed by the formula:

0.5 to 1.5 R_2O : Y_2O_3 : at least 10 XO_2 : 0 to 100 H_2O

wherein R is a monovalent cation or 1/n of a cation of valency n, X is silicon and/or germanium, Y is one or more of aluminium, iron, gallium or boron, and H_2O is water of hydration additional to water notionally present when R is H, and having an X-ray pattern substantially as set out in Tables 1 and 2 (as determined by standard technique using copper $K\alpha$ radiation).

Table 1 shows X-ray data for zeolite EU-1 as prepared, and

15 Table 2 shows X-ray data for zeolite EU-1 in the calcined Na-H form. The X-ray pattern is little affected by the type of cation present.

TABLE 1
Zeolite EU-1 as freshly prepared

d (A)	I/I ₀
11.03	Very Strong
10.10	Strong
9.72	Weak
6.84	Weak
5.86	Very Weak
4.66	Very Strong
4.31	Very Strong
4.00	Very Strong
3.82	Strong
3.71	Strong
3.44	Medium
3.38	Medium
3.26	Strong
3.16	Very Weak
3.11	Very Weak
2.96	Very Weak
2.71	Very Weak
2.55	Weak
2.48	Very Weak
2.42	Very Weak
2.33	Very Weak
2.30	Very Weak
2.13	Very Weak

TABLE 2

Zeolite EU-1 in calcined Na-H form

d (A)	I/I ₀
11.11	Very strong
10.03	Very strong
9.78	Weak
7.62	Weak
6.84	Medium
6.21	Very Weak
5.73	Weak
4.87	Very weak
4.60	Very strong
4.30	Very strong
3.97	Very strong
3.77	Strong
3.71	Weak
3.63	Very weak
3.42	Medium
3.33	Medium
3.27	Strong
3.23	Medium
3.15	Weak
3.07	Weak
2.93	Weak
2.69	Weak
2.63	Very weak
2.57	Very weak
2.51	Weak
2.45	Very weak
2.41	Very weak
2.32	Very weak
2.29	Very weak
2.11	Very weak

Within the above definition of chemical composition, the number of moles of XO_2 is typically in the range 10 to 500 and zeolite EU-1 appears to be most readily formed in a state of high purity when the number of moles of XO_2 is in the range 20 to 300.

This definition includes both freshly prepared zeolite EU-1 ("freshly prepared" means the product of synthesis and washing, with optional drying, as hereinafter described) and also forms of it resulting from dehydration, and/or calcination, and/or ion exchange. In freshly prepared zeolite EU-1, R may include an alkali metal cation; especially sodium, and/or ammonium, and usually or when prepared from alkylated nitrogen compounds, includes nitrogen-containing organic cations as described below or cationic degradation products thereof, or precursors thereof. These nitrogen containing cations are hereinafter referred to as Q.

The freshly prepared zeolite EU-1 may also contain nitrogen-containing compounds well in excess of the 1.5 moles set out in the aforesaid definition of the composition of zeolite EU-1, typically in the range 0.1 to 20 moles per mole of Y_2O_3 . Since EU-1 is a zeolite, the excess nitrogen-containing base must be physically trapped within the crystal lattice, because it is too large to escape. It can only be removed by thermal or oxidative degradation. This physically trapped basic material does not constitute part of the composition for the purposes of the definition. Thus a zeolite EU-1 as made typically has the following molar composition:

0 to 0.8 M_2O : 0.1 to 20 Q : Y_2O_3 : 10 to 500 XO_2 : 0 to 100 H_2O wherein M is an alkali metal or ammonium, and $M_2O + Q \geq 1.0$

The H_2O content of freshly prepared zeolite EU-1 depends on the conditions in which it has been dried after synthesis.

In calcined forms of zeolite EU-1, R may be alkali

metal but includes less or no nitrogen-containing organic compounds, since these are burnt out in the presence of air, leaving hydrogen as the other balancing cation.

Among the ion-exchanged forms of zeolite EU-1 the 5 ammonium (NH_4^+) is of importance since it can be readily converted to the hydrogen form by calcination. The hydrogen form can also be prepared directly by exchange with an acid. The hydrogen-form and forms containing metals introduced by ion exchange are described further below.

10 We believe that zeolite EU-1 is similar to the ZSM-23 family of zeolites (as described for example, in US Patent 4,076,842, although our attempts to make ZSM-23 in accordance with this and other published descriptions have so far been unsuccessful). An analogy can be drawn 15 with the relationship between the aforesaid ZSM-23 family of zeolites and the ZSM-5/ZSM-11 family of zeolites (as described, for example in US Patents 3,702,886 and 3,709,979; and in Nature, 1978, 275, 119), which from the literature appear to have similar X-ray diffraction data, but in fact 20 have related, but significantly different, three dimensional frameworks.

Zeolite EU-1 has molecular sieve properties analogous to those of known zeolites. Thus zeolite EU-1 may be characterised by its adsorption capacity for molecules of 25 various sizes. Typical results are shown in Table 3. Slight sorption of cyclohexane and rapid sorption of p-xylene suggest an entry port size of about 6.0 Å in diameter. The results given in Table 3 also show that m-xylene is sorbed more slowly than p-xylenes, thereby indicating that zeolite 30 EU-1 may be used to separate xylene isomers. It will also be seen from Table 3 that zeolite EU-1 has significant hydrophobic voidage, the voids volume available for water being only 6.9 cc per 100 g as compared with 14.4 cc per 100 g for n-hexane and 12.4 cc per 100 g for p-xylene. 35 This means that zeolite EU-1 is a useful sorbent for removing hydrocarbons from wet gas or from aqueous effluents.

TABLE 3 - Sorption at 25°C

Adsorbate	Kinetic* Diameter Å	Pressure mm Hg	Time Hours	Wt sorbed g/100 g	Voidage available cc/100 g
Water	2.7	4.5	2	6.9	6.9
	2.7	4.5	16	11.0	11.0
n-hexane	4.3	45.8	2	9.5	14.4
p-xylene	5.8	1.6	2	10.5	12.1
	5.8	1.6	18.5	10.6	12.2
m-xylene	5.9	1.6	2	2.3	2.6
			18.5	5.5	6.3
cyclohexane	6.0	2.7	2	1.1	1.4
			18.5	1.1	1.4

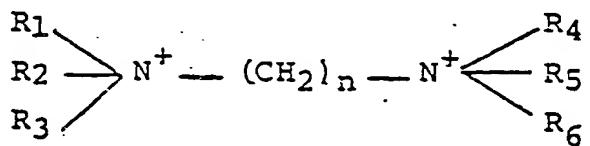
* Lennard Jones kinetic diameter
see D W Breck "Zeolite Molecular Sieves", Wiley Interscience, 1974 p 636

Zeolite EU-1 is further characterised by its infrared spectrum (shown in Figure 1). In common with other zeolites, zeolite EU-1 has two main IR absorption regions, viz. the stretch ν of the Si-O situated near to 1100 cm^{-1} and the deformation δ of the Si-O situated near to 500 cm^{-1} .

Referring to the absorption near to 1100 cm^{-1} , zeolite EU-1 has absorptions at 1213 cm^{-1} (medium weak intensity) and at 1080 cm^{-1} (very strong). By comparison, the absorptions near 1100 cm^{-1} for zeolites ZSM-5 and ZSM-11 are 1228 cm^{-1} (medium) and 1095 cm^{-1} (very strong) for ZSM-5, and 1221 cm^{-1} (medium strong) and 1090 cm^{-1} (very strong) for ZSM-11. Thus there are small but significant differences both in position and intensity of the absorption of zeolite EU-1 as compared with the absorptions of ZSM-5 and ZSM-11.

The deformation δ near to 500 cm^{-1} of EU-1 has a medium intensity absorption band which is a doublet centred at 570 cm^{-1} and which is much weaker than the band at 470 cm^{-1} . By comparison, ZSM-11 has a doublet which is symmetrically shaped with absorption occurring at 548 cm^{-1} and 448 cm^{-1} . ZSM-5 has a doublet absorption band at 545 cm^{-1} and a second band at 455 cm^{-1} . Thus EU-1 is similar to ZSM-5 in that the higher absorption centred at 570 cm^{-1} is a doublet. However, the shifts in position, number and relative intensities of the absorptions at 500 cm^{-1} (and at 1100 cm^{-1} as described above) are sufficient to identify EU-1 and to distinguish it from ZSM-5 and ZSM-11.

The invention provides also a method of making zeolite EU-1 which comprises reacting an aqueous mixture comprising at least one oxide XO_2 , at least one oxide Y_2O_3 , and at least one alkylated derivative of a polymethylene α - ω diamine having the formula



which by our definition is Q^{2+}

an amine degradation product thereof, or a precursor thereof, wherein n is in the range from 3 to 12 and R_1 to R_6 which may be the same or different, can be alkyl or hydroxyalkyl groups, containing from 1 to 8 carbon atoms and up to five of the groups R_1 - R_6 can be hydrogen, the mixture having the molar composition:

XO_2/Y_2O_3	at least 10, preferably 10 to 150
OH^-/XO_2	0.1 to 6.0 preferably 0.1 to 1.0
10 $(M^+ + Q)/Y_2O_3$	0.5 to 100
$Q/(M^+ + Q)$	0.1 to 1.0
H_2O/XO_2	1 to 100

where X is silicon and/or germanium, Y is one or more of aluminium, iron, gallium, or boron, M is an alkali metal or ammonium, and Q is the aforesaid alkylated derivative of a polymethylene diamine, an amine degradation product thereof, or a precursor thereof, or a related compound.

20 M and/or Q can be present as hydroxides or salts of inorganic or organic acids provided the OH^-/XO_2 requirement is fulfilled.

Preferred alkylated polymethylene diamine starting materials include alkylated hexamethylene diamines, especially methylated hexamethylene diamines, for example 25 1:6 N,N,N,N^1,N^1,N^1 -hexamethyl hexamethylene diammonium salts (e.g. halide, hydroxide, sulphate, silicate, aluminate).

Suitable precursors of the alkylated polymethylene diamine starting materials include the parent diamine along 30 with alcohols or alkyl halides which can be used as such or can be preheated together in the reaction vessel preferably in solution (e.g. in methyl ethyl ketone) prior to addition of the other reactants required for zeolite EU-1 synthesis.

The preferred alkali metal (M) is sodium. The 35 preferred oxide XO_2 is silica (SiO_2) and the preferred oxide Y_2O_3 is alumina (Al_2O_3).

The silica source can be any of those commonly

considered for use in synthesising zeolites, for example powdered solid silica, silicic acid, colloidal silica or dissolved silica. Among the powdered silicas usable are precipitated silicas, especially those made by precipitation 5 from an alkali metal silicate solution, such as the type known as "KS 300" made by AKZO, and similar products, aerosil silicas, fume silicas and silica gels suitably in grades for use in reinforcing pigments for rubber or silicone rubber. Colloidal silicas of various particle 10 sizes may be used, for example 10-15 or 40-50 microns, as sold under the Registered Trade Marks "LUDOX", "NALCOAG" and "SYNTON". The usable dissolved silicas include commercially available waterglass silicates containing 0.5 to 6.0, especially 2.0 to 4.0 mols of SiO_2 per mol of 15 alkali metal oxide, "active" alkali metal silicates as defined in UK Patent 1193254, and silicates made by dissolving silica in an alkali metal hydroxide or quaternary ammonium hydroxide or a mixture thereof.

The alumina source is most conveniently sodium 20 aluminate, but aluminium, an aluminium salt, for example the chloride, nitrate or sulphate, an aluminium alkoxide or alumina itself, which should preferably be in a hydrated or hydratable form such as colloidal alumina, pseudohohemite, boehmite, gamma alumina or the alpha or beta trihydrate.

The reaction mixture is usually reacted under autogenous pressure, optionally with added gas, e.g. nitrogen, at a temperature between 85 and 250°C until crystals of zeolite EU-1 form, which can be from 1 hour 5 to many months depending on the reactant composition and the operating temperature. Agitation is optional, but is preferable since it reduces the reaction time.

At the end of the reaction, the solid phase is collected on a filter and washed and is then ready for 10 further steps such as drying, dehydration and ion-exchange.

If the product of the reaction contains alkali metal ions, these have to be at least partly removed in order to prepare the hydrogen form of EU-1 and this can be done by ion exchange with an acid, especially a strong 15 mineral acid such as hydrochloric acid or by way of the ammonium compound, made by ion exchange with a solution of an ammonium salt such as ammonium chloride. Ion exchange can be carried out by slurring once or several times with the ion-exchange solution. The zeolite is usually calcined 20 after ion exchange but this may be effected before ion-exchange or during ion-exchange if the latter is carried out in a number of stages.

In general, the cation(s) of zeolite EU-1 can be replaced by any cation(s) of metals, and particularly 25 those in Groups IA, IB, IIA, IIB, III (including rare earths) VIII (including noble metals) and by lead, tin and bismuth. (The Periodic Table is as in "Abridgements of Specifications" published by the UK Patent Office). Exchange is carried out using any water soluble salts 30 containing the appropriate cation.

When used as a catalyst, zeolite EU-1 can be associated with an inorganic matrix, which can be either inert or catalytically active. The matrix may be present simply as a binding agent to hold the small zeolite 35 particles (0.005 to 10 microns) together, or it may be added as a diluent to control the amount of conversion in a process which may otherwise proceed at too

high a rate, leading to catalyst fouling as a result of excessive coke formation. Typical inorganic diluents include catalyst support materials such as alumina, silica and kaolinic clays, bentonites, montmorillonites, sepiolite, 5 attapulgite, Fullers earth, synthetic porous materials such as $\text{SiO}_2\text{-Al}_2\text{O}_3$, $\text{SiO}_2\text{-ZrO}_2$, $\text{SiO}_2\text{-ThO}_2$, $\text{SiO}_2\text{-BeO}$, $\text{SiO}_2\text{-TiO}_2$ or any combination of these diluents. An effective way of 10 mixing zeolite EU-1 with such diluents is to mix appropriate aqueous slurries in a mixing nozzle and then to spray-dry the slurry. Other ways of mixing can be used.

If zeolite EU-1 in any cationic form or as a catalytic composite is exchanged or impregnated with hydro- 15 genation/dehydrogenation components, such as Ni, Co, Pt, Pd, Re, Rh, hydrocracking and reforming catalysts can be made, especially if the Na_2O content is less than 0.1% w/w.

A wide range of hydrocarbon conversion catalysts 20 can be prepared from zeolite EU-1 by ion exchange or impregnation with cations, or oxides, selected from the following, Cu, Ag, Mg, Ca, Sr, Zn, Cd, B, Al, Sn, Pb, V, P, Sb, Cr, Mo, W, Mn, Re, Fe, Co, Ni, noble metals.

Usually the EU-1 catalyst will be in acid form, thus stoichiometry is maintained by H^+ or H_3O^+ as an additional balancing cation, or as sole cation. Such 25 catalysts may find application in the following processes; catalytic cracking, hydrodesulphurization, hydrodenitri- fication, catalytic dewaxing, alkylation of alkanes or aromatics, dealkylation, disproportionation, isomerisation of alkanes and alkyl benzenes, dehydration reactions, 30 oxidation and polymerisation.

We have found that zeolite EU-1 is especially useful as a catalyst for xylenes isomerisation. As is well known, the major aim in xylenes isomerisation is to increase the para-xylene content of the feedstock at the 35 expense of other isomers since para-xylene is a particularly useful and valuable product. The mixed xylenes feedstocks

commonly available for xylenes isomerisation usually contain amounts of the three xylene isomers as well as ethylbenzene. Hitherto, some of the mixed xylenes feedstock available has contained relatively small amounts of ethylbenzene but it is anticipated that in the future such feedstocks will become more expensive and that resort will have to be made to feedstocks containing rather larger amounts of ethylbenzene, say up to about 25% ethylbenzene.

According to a further aspect of the present invention we provide a hydrocarbon conversion process which comprises contacting an alkylbenzene or a mixture of alkylbenzenes under isomerisation conditions in the vapour or liquid phase with a catalyst comprising EU-1.

The EU-1 zeolite may conveniently be used as an aggregate in the form of pellets or extrudates, and a dispersing medium, for example gamma-alumina, may be used in the aggregates.

In the vapour phase suitable isomerisation conditions include a temperature in the range 100-600°C, preferably 200-450°C, a pressure in the range 0.5-50, preferably 1-5 atm abs, and a weight hourly space velocity (WHSV) up to 80, or even higher if desired. These conditions are used preferably in the absence of added free hydrogen and with EU-1 containing no hydrogenation/dehydrogenation component.

In the liquid phase suitable isomerisation conditions include a temperature in the range 0-350°C, a pressure in the range 1-200, preferably 5-70 atm abs., and, in a flow system, a weight hourly space velocity (WHSV) preferably in the range 1 to 30, the higher flow rates being used at the higher temperature. Optionally a diluent is present, suitably one or more of those having a critical temperature higher than the isomerisation temperature being used and including toluene, trimethylbenzene, naphthenes and paraffins. Preferably the diluent if present amounts to 1-90% w/w of the feed to the isomerisation reaction. In this liquid phase process the catalyst also preferably

contains no hydrogenation/dehydrogenation component and no added free hydrogen is present.

Optionally isomerisation in the vapour phase is conducted in the presence of hydrogen. A suitable mole 5 ratio of hydrogen to alkylbenzene lies in the range 3 to 30:1. If hydrogen is used, the catalyst should comprise a hydrogenation/dehydrogenation component, preferably a metal of Group VIII of the Periodic Table, especially platinum or nickel. The amount of metal preferably lies 10 in the range 0.1 to 2% w/w on the total catalyst. If desired, the catalyst may contain one or more additional metals, for example, rhenium, suitably in the range 0.1 to 2% w/w on the total catalyst.

Preferably the alkylbenzene is a xylene, for 15 example, m-xylene for conversion to p-xylene, or a mixture of xylenes, possibly with ethylbenzene. The amount of ethylbenzene present will depend to some extent on the source of the xylene mixture but will usually lie in the range 0 to 25% w/w, especially 6 to 25% w/w of the feed- 20 stock, since the process is able to handle feeds containing relatively high amounts of ethylbenzene.

If desired, the EU-1 catalyst used in the process of the invention may contain small amounts of alkali metal, for example up to 1000 and especially up to 300 ppm w/w 25 as equivalent Na₂O. It appears to be unnecessary to have present ions other than hydrogen and (for hydro-isomerisation) Group VIII metal ions. The EU-1 may contain onium compounds and their decomposition products to the extent of 0.05 to 1.0% w/w such as are present after substantial removal of 30 such materials by calcination in air, when it is to be used in xylenes isomerisation.

Zeolite EU-1 may also find applications in the separation of aromatics and cycloparaffins, and in pollution control by its ability to remove organic contaminants from 35 aqueous effluents.

The invention is illustrated by the following Examples.

Example 1

Preparation of sodium hexamethonium EU-1 and sodium hydrogen EU-1

The synthesis mixture had the following molar composition:

5	Na ₂ O	7.5
	Hx Br ₂	7.5
	Al ₂ O ₃	1.0
	SiO ₂	43
	H ₂ O	2220

10 Hx Br₂ = hexamethonium bromide = $\text{Me}_3\text{N}(\text{CH}_2)_6\text{NMe}_3^{2+} (\text{Br}^-)_2$
 Solid silica (36 g of AKZO grade KS 300 of composition 5.09
 Na₂O, Al₂O₃, 728 SiO₂, 248 H₂O) was suspended in a mixture
 of 34 g hexamethonium bromide and 468 g water. Next 6 g
 15 solid sodium hydroxide, and 2.8 g solid sodium aluminate
 (1.25 Na₂O, Al₂O₃, 3H₂O) were dissolved in 35 g water and
 stirred into the silica suspension. The resulting slurry
 was reacted in a stainless steel autoclave stirred at
 800 rpm for 22.5 hours at 200°C under autogenous pressure.
 After cooling to about 60°C, the slurry product was
 20 filtered and washed with 2 litres of distilled water at
 60°C, and dried overnight at 120°C. The product was
 sodium hexamethonium EU-1, along with a small quantity of
 alphaquartz, had the X-ray data shown in Table 1, and the
 composition 0.8 Na₂O, 5.5 Q, Al₂O₃, 35 SiO₂, 10 H₂O where
 25 Q²⁺ is hexamethonium i.e. for correct stoichiometry
 $\frac{1}{2} [\text{O} [\text{N}(\text{CH}_3)_3\text{N}-(\text{CH}_2)_6-\text{N}(\text{CH}_3)_3]_2 \text{O}]$, and crystallite sizes
 of 1 to 3 microns.

This product was calcined in air for 48 hours at
 450°C and was found to have an X-ray diffraction pattern
 30 as shown in Table 2 and a nitrogen and carbon content of
 less than 0.1% w/w. This product was sodium hydrogen EU-1.

Example 2

Preparation of hydrogen EU-1

The calcined product of Example 1 was slurry-exchanged for
 35 1 hour at 25°C with 3.6 ml of N hydrochloric acid per g.
 of zeolite. The resulting hydrogen EU-1 zeolite was washed
 with 10 ml distilled water per g. of zeolite, dried over-

night at 120°C and activated for sorption and catalyst testing at 450°C, for 6 hours.

Examples 3-11

The synthesis procedure of Example 1 was repeated using a range of reactants, mixture compositions, reaction temperatures and reaction times. The results are shown in Table 4.

TABLE 4

Ex.	Organic Component	Silicon Component	Reaction Mixture Composition - moles					Temp °C	Time hours	Product
			Na ₂ O	Q	Al ₂ O ₃	SiO ₂	H ₂ O			
3	Hx Br ₂	KS 300	10	10	1	60	3000	180	168	major EU-1 (1)
4	Hx Br ₂	KS 300	10	10	1	86	3000	150	168	major EU-1 (2)
5	Hx Br ₂	CAB-O-SIL M5	20	20	1	120	6000	180	168	major EU-1
6	Hx Br ₂	CAB-O-SIL M5	10	10	1	60	3000	220	3.75	major EU-1
7	Hx Cl ₂	KS 300	7.5	7.5	1	45	2200	200	22	major EU-1 (3)
8	Hx Cl ₂	KS 300	7.5	7.5	1	45	2200	200	39	major EU-1 (3)
9	Hx Br ₂	CAB-O-SIL M5	10	10	1	60	3000	200	6.5 (4)	major EU-1
10	Hx Br ₂	CAB-O-SIL M5	10	10	1	60	3000	200	4.0 (5)	major EU-1
11	Hx Br ₂	CAB-O-SIL M5	10	10	1	60	2000	200	8	major EU-1 + trace quartz
12	Hx Br ₂	CAB-O-SIL M5	10+10 (6)	10	1	60	3000	180	5	major EU-1 + trace quartz
13	Hx Br ₂	CAB-O-SIL M5	10	7+3 (7)	1	60	3000	180	5	major EU-1 + trace quartz

Notes on Table 4

Hx Br₂ = hexamethonium bromide
 Hx Cl₂ = hexamethonium chloride
 KS 300 = silica (AKZO grade KS 300)
 CAB-O-SIL M5 = silica (Cabot Carbon fume silica)

(1) EU-1 product SiO₂/Al₂O₃ = 45.7
 (2) EU-1 product SiO₂/Al₂O₃ = 76.8
 (3) EU-1 product SiO₂/Al₂O₃ = 32.0
 (4) Stirrer speed 300 rpm
 (5) Stirrer speed 750 rpm
 (6) 10 moles Na₂O + 10 moles NH₄OH
 (7) 7 moles Hx Br₂ + 3 moles hexamethylene diamine

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Example 14

Example 3 was repeated except that hexamethonium bromide was replaced by a chemical equivalent of decamethonium bromide. The product after 150 hours at 180°C was

5 zeolite EU-1 plus minor amounts of an unknown crystalline impurity.

Examples 15-17

A sample of zeolite EU-1 (prepared as described in Example 1) was formed into aggregates of 425 to 1000 µm.

10 Three samples of aggregates (Examples 15-17) were tested as xylenes isomerisation catalysts as follows:

Each sample was charged to a glass reactor and heated in a stream of air at 500°C for 16 hours. It was then cooled in a nitrogen stream to reaction temperature.

15 A feedstock consisting mainly of aromatic hydrocarbons was then passed over the sample at atmospheric pressure for 6 hours.

For comparison, (Example A) a 12 g sample of an amorphous silica/alumina catalyst in the form of 3-5 mm

20 beads containing 10% alumina was charged to a glass reactor and treated in the same manner.

The composition of the feedstock is shown in Table 5. The reaction conditions used and the product composition after 6 hours on line are shown for each

25 sample of EU-1 and for the silica/alumina catalyst in Table 6.

TABLE 5

Component	Weight (%)
Benzene	0.02
Toluene	1.87
Ethylbenzene	8.56
Para-xylene	7.63
Meta-xylene	50.58
Ortho-xylene	26.02
C ₉ + aromatics	3.91

TABLE 6

Example	15	16	17	A
Catalyst	EU-1	EU-1	EU-1	SiO ₂ /Al ₂ O ₃
Temperature (°C)	450	450	400	450
WHSV	13	84	59	1
Product Composition (wt %)				
Benzene	0.69	0.20	0.10	0.53
Toluene	3.69	2.06	2.03	4.19
Ethylbenzene	6.67	8.34	8.35	7.46
Para-xylene	19.75	19.65	17.22	17.28
Meta-xylene	42.51	43.58	44.38	41.90
Ortho-xylene	19.39	20.82	22.46	20.78
C ₉ + aromatics	6.41	4.11	4.08	6.59
% Ethylbenzene loss	22.1	2.6	2.4	12.8
% Xylene loss	3.1	0.2	0.2	5.1

20 Referring to Table 6, Example 15 shows that EU-1 catalyst can produce a higher percentage of para-xylene in the product, a greater ethylbenzene loss and less xylenes destruction at a higher space velocity than the amorphous silica/alumina catalyst (Comparative Example A).

25 Example 16 shows that at a higher space velocity EU-1 catalyst can still give a high percentage of para-xylene in the product with very little xylenes loss.

30 Example 17 shows that at a 50°C lower reaction temperature and a much higher space velocity than that used in Example 16, EU-1 catalyst can still give the same percentage of para-xylene in the product as does the silica/alumina catalyst but with very little xylenes loss.

What we claim is:

1. Zeolite EU-1 having a molar composition expressed by the formula:

0.5 to 1.5 R_2O : Y_2O_3 : at least 10 XO_2 : O to 100 H_2O wherein R is a monovalent cation or 1/n of a cation of valency n, X is silicon and/or germanium, Y is one or more of aluminium, iron, gallium or boron, and H_2O is water of hydration additional to water notionally present when R is H, and having, when freshly prepared, an X-ray diffraction pattern substantially as shown in Table 1.

2. Zeolite EU-1 according to claim 1 wherein the molar composition is expressed by the formula:

0.5 to 1.5 R_2O : Y_2O_3 : 20 to 300 XO_2 : O to 100 H_2O .

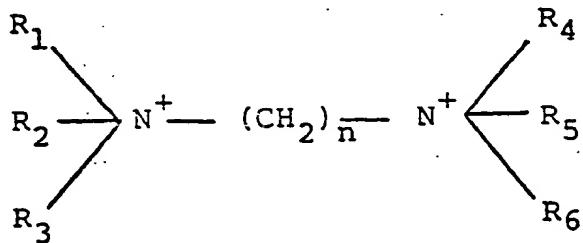
3. Zeolite EU-1 according to claim 1 or claim 2 wherein R is or includes hydrogen.

4. Zeolite EU-1 according to claim 1 as freshly made having a molar composition expressed by the formula:

0 to 0.8 M_2O : 0.1 to 20 Q : Y_2O_3 : 10 to 500 XO_2 : O to 100 H_2O

wherein M is an alkali metal or ammonium, Q is a nitrogen-containing organic cation and $M_2O + Q \geq 1.0$.

5. A method of making zeolite EU-1 as defined in claim 1 which comprises reacting an aqueous mixture comprising at least one oxide XO_2 , at least one oxide Y_2O_3 and at least one alkylated derivative of a polymethylene α - ω diamine having the formula:



an amine degradation product thereof, or a precursor thereof, wherein n is in the range from 3 to 12 and R₁ to R₆ which may be the same or different, can be alkyl

or hydroxyalkyl groups containing from 1 to 8 carbon atoms and up to five of the groups R_1 - R_6 can be hydrogen, the mixture having the molar composition:

XO_2/Y_2O_3	at least 10
OH^-/XO_2	0.1 to 6.0
$(M^+ + Q)/Y_2O_3$	0.5 to 100
$Q/(M^+ + Q)$	0.1 to 1.0
H_2O/XO_2	1 to 100

where X is silicon and/or germanium, Y is one or more of aluminium, iron, gallium, or boron, M is an alkali metal or ammonium, and Q is the aforesaid alkylated derivative of a polymethylene diamine, an amine degradation product thereof, or a precursor thereof.

6. A method according to claim 5 wherein XO_2/Y_2O_3 is in the range 10 to 150.

7. A method according to claim 5 or claim 6 wherein OH^-/XO_2 is in the range 0.1 to 1.0.

8. A method according to any one of claims 5 to 7 wherein the alkylated derivative of a polymethylene diamine is an alkylated hexamethylene diamine.

9. A method according to claim 8 wherein the alkylated hexamethylene diamine is an N, N, N, N^1, N^1 -hexamethyl-1,6-hexamethylene diammonium salt.

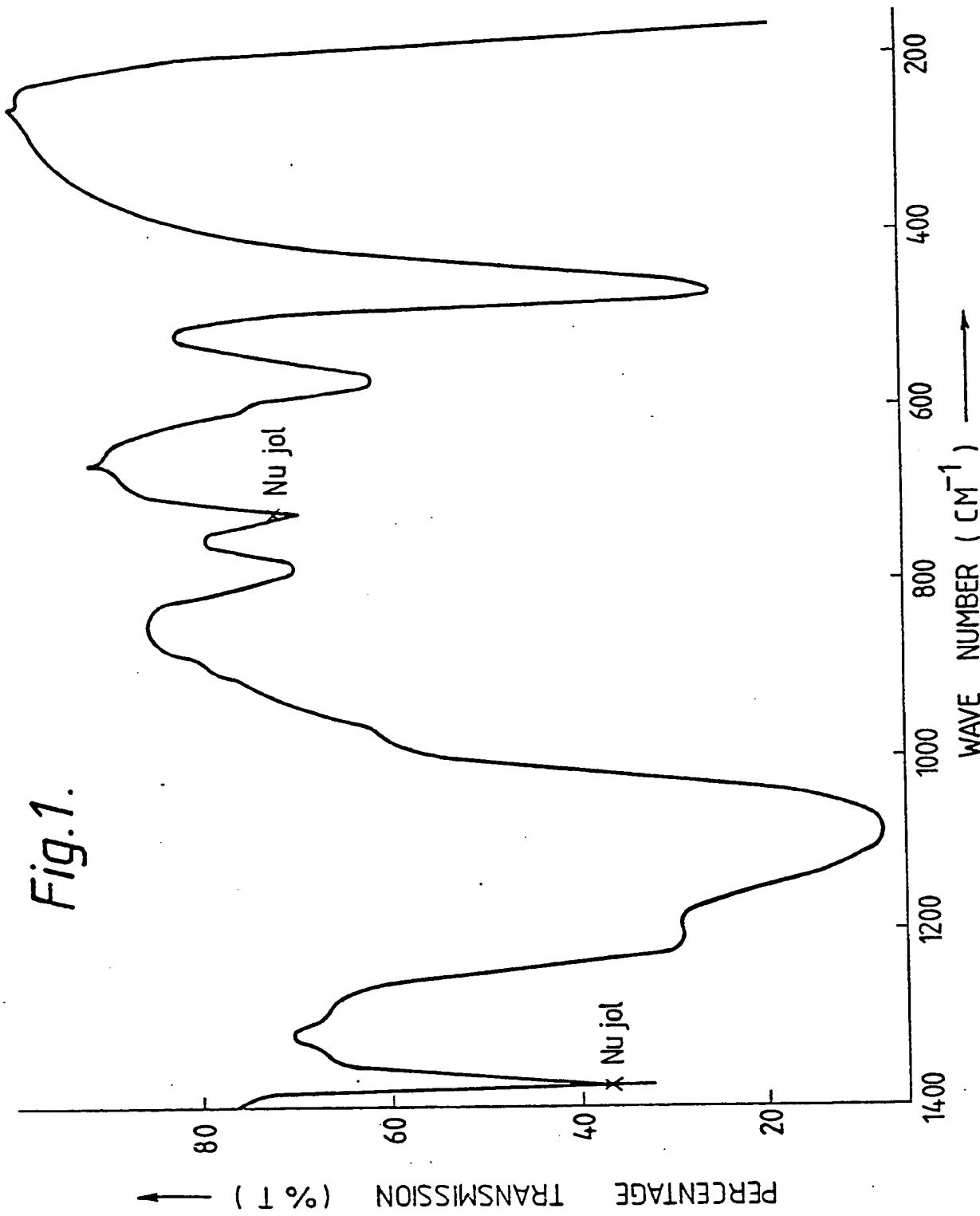
10. A catalyst comprising zeolite EU-1 as claimed in any one of claims 1 to 4.

11. A catalytic process employing the catalyst claimed in claim 10.

12. A process according to claim 11 wherein an alkylbenzene or a mixture of alkylbenzenes is contacted with the catalyst under isomerisation conditions.

13. A process according to claim 12 wherein the alkylbenzene or mixture of alkylbenzenes comprises a xylene or a mixture of xylenes.

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DOCUMENTS CONSIDERED TO BE RELEVANT			CLASSIFICATION OF THE APPLICATION (Int. Cl.)
Category	Citation of document with indication, where appropriate, of relevant passages	Relevant to claim	
	<p><u>EP - A1 - 0 000 669</u> (MOBIL OIL) * claims 1, 5 *</p> <p>---</p> <p><u>EP - A1 - 0 007 081</u> (BASF) * claim 1 *</p> <p>---</p>	5	<p>C 01 B 33/28</p> <p>B 01 J 29/04</p> <p>C 07 C 5/22</p>
D	<u>US - A - 4 076 842</u> (C.J. PLANK et al.)	5	TECHNICAL FIELDS SEARCHED (Int. Cl.)
D	<u>US - A - 3 709 979</u> (P. CHU)	5	
D	<u>US - A - 3 702 886</u> (R.J. ARGAUER et al.)	5	C 01 B 33/00
D	<u>GB - A - 1 193 254</u> (P. SPENCE & SONS)	5	
			CATEGORY OF CITED DOCUMENTS
			<p>X: particularly relevant</p> <p>A: technological background</p> <p>O: non-written disclosure</p> <p>P: intermediate document</p> <p>T: theory or principle underlying the invention</p> <p>E: conflicting application</p> <p>D: document cited in the application</p> <p>L: citation for other reasons</p>
X	The present search report has been drawn up for all claims		<p>& member of the same patent family,</p> <p>corresponding document</p>
Place of search	Date of completion of the search	Examine-	
Berlin	14-08-1981	KESTEN	

